

Removal of Sulfur in Petroleum Refining Using DCS

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Abstract: - Petroleum refining area Sulfur is naturally present as an impurity in fossil fuels. When the fuels are burned, the sulfur is Released as sulfur dioxide—an air pollutant responsible for respiratory problems and acid rain. Environmental regulations have increasingly restricted sulfur dioxide emissions, forcing fuel Processors to remove the sulfur from both fuels and exhaust gases. The cost of removing sulfur from natural gas and petroleum is high. In natural gas, sulfur is present mainly as hydrogen sulfide gas (H₂S), while in crude oil it is present in sulfur-containing organic compounds which are converted into hydrocarbons and H₂S during the removal process (hydro desulfurization). This well-established process uses partial combustion and catalytic oxidation to convert about 97% of the H₂S to elemental sulfur. Implement **Distributed Control System (DCS) CENTUM CS3000** to automate the removal process in petroleum refining.

Keywords: - DCS, Valve, Parameters, Automation

I. INTRODUCTION

Hydrodesulfurization(HDS) is a catalytic chemical process widely used to remove sulfur (S) from natural gas and from refined petroleum products such as gasoline or petrol, jet fuel, kerosene, diesel, and fuel oils. The purpose of removing the sulfur is to reduce the sulfur dioxide (SO₂) emissions that result from using those fuels in automotive vehicles, aircraft, locomotives, ships, gas or oil burning power plants, residential and industrial furnaces, and other forms of fuel combustion. Another important reason for removing sulfur from the naphtha streams within a petroleum refinery is that sulfur, even in extremely low concentrations, poisons the noble metal catalysts (platinum and rhenium) in the catalytic reforming units that are subsequently used to upgrade the octane rating of the naphtha streams[3]. The industrial hydrodesulfurization processes include facilities for the capture and removal of the resulting hydrogen sulfide (H₂S) gas. In petroleum refineries, the hydrogen sulfide gas is then subsequently converted into by product elemental sulfur or sulfuric acid (H₂SO₄).

II. OBJECTIVE

The main objective of the project is to Design and Develop a Removal of sulfur in petroleum refining using DCS Integration. Programming the system in DCS using function block diagram. To remove the sulfur in natural gas, diesel, petrol, for emission control process. The industrial hydrodesulfurization processes include facilities for the capture and removal of the resulting hydrogen sulfide (H₂S) gas. Finally the hydrogen sulfide gas is then subsequently converted into by product elemental sulfur or sulfuric acid (H₂SO₄). Yokogawa has developed software for DCS control system named it as CENTUM CS3000[1]. DCS can handle vast amount of process data and can be configured without major changes in software and hardware architecture.

III. PROCESS DESCRIPTION

Hydrodesulfurization (HDS) is a catalytic chemical process widely used to remove sulfur (S) from natural gas and from refined petroleum products such as gasoline or petrol, jet fuel, kerosene, diesel, and fuel oils. The purpose of removing the sulfur is to reduce the sulfur dioxide (SO₂) emissions that result from using those fuels in automotive vehicles, aircraft, railroad locomotives, ships, gas or oil burning power plants, residential and industrial furnaces, and other forms of fuel combustion. Another important reason for removing sulfur from the naphtha streams within a petroleum refinery is that sulfur, even in extremely low concentrations, poisons the noble metal catalysts (platinum and rhenium) in the catalytic reforming units that are subsequently used to upgrade the octane rating of the naphtha streams.

The industrial hydrodesulfurization processes include facilities for the capture and removal of the resulting hydrogen sulfide (H₂S) gas. In petroleum refineries, the hydrogen sulfide gas is then subsequently converted into by product elemental sulfur or sulfuric acid (H₂SO₄). In fact, the vast majority of the 64,000,000 metric tons of sulfur produced worldwide in 2005 was by-product sulfur from refineries and other hydrocarbon processing plants. An HDS unit in the petroleum refining industry is also often referred to as a **hydrotreater**

2) Sequence table block (ST-16):

This is a decision table type function block that describes the relationship between input signal and output signal in Y/N (yes/no) fashion.

3) Relational expression block (RL):

This is based on the comparison of two values. All the values need to be compared is written in the RL block and then invoked in sequence table and select the operator as CMP for comparison of values.

4) CALCU Block:

Calculation block receives analog values or digital values as input values, and perform calculation according to these parameters. The result of calculation is outputted as calculated output value (CPV). B. Major control loops identified and its programming The control loops are grouped into common and similar loops, accordingly the following are the control logics used in desalting process control;

1) Temperature Measuring Logic:

This is a simple open loop logic used for communicating temperature at various distributed level for measurement and indications. A thermal field instrument is responsible of measuring and transmitter transmits thermal data to DCS on demand. The demand is enabled by request from the DCS and is indicated in the indicator for process value.

2) Pressure Measuring Logic:

The pressure measuring logic is a simple open loop logic used for communicating pressure at various distributed level for measurement and indications. A pressure detecting gauge is responsible of measuring and transmitting pressure data on demand from DCS. The demand is enabled by request from the DCS and is indicated in the indicators.

3) Flow Control Logic:

The valve control is made either to control flow rate in the pipe or to control level of fluid in the tank. The flow control logic has a flow transmitter that in turn communicates with DCS controller. The controller takes actuation on valve depending on the set value as prescribed by the operator. The manipulated value (MV) is automatically enforced on the control actuator by the PID controller depending on the set value (SV) and the process value (PV). The controller finally adjusts the PV to the SV during load fluctuations.

4) Mode Change Logic:

The mode change logic is very important redundancy technique. When the DCS limit is reached or is out of range then the mode is shifted between manual and auto modes for automatic or manual control. The range and the conditions are user specified and can be programmed. The range of values is process values as measured by field instruments.

5) Motor Control Logic for a Pump: Motor control is very important device control logic for flow control through the pump at process activity station with safety. A motor control block has open and close positions for operating motor at DCS control station and to start, stop and trip motor. Safety switches and alternatives switches are also provided to ensure safety.

6) Two out of Three Voting Logic: Two out of three voting logic can be used in any instrumentation system, which achieves two important things; If there is a problem in a system, it increases the chances of detecting it and taking remedial action. It reduces the chances of taking action (shutting down of system) when there is not really a problem.

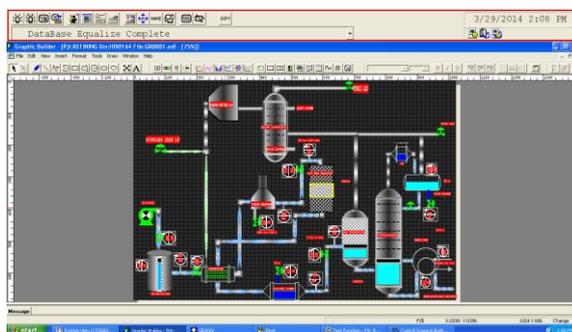


Figure 2: Screen Printout of Plant Control Graphic Window

7) Programming of Two out of Three Voting Logic for Power Control:

The CALCU block evaluates the state of the three indicators. There are three inputs LT004A, LT004B and LT004C which are indicated in variables INDA51, INDB51 and INDC51 respectively. If INDC51 is more than 10% error, this variable is voted out and the average of INDA51 and INDB51 is sent as output value and an

alarm message will be displayed with buzzer that INDC51 is voted out. If all are within range of error and alarm message will be displayed as reliable. If all are in discrepancy then the controller will shift to manual mode.

The process Control Graphic Window (CGW) is important in Human Interface System (HIS), which allows operator to monitor and navigate through various process parameters in real time and take necessary decision and action according to the situations in the process control. The graphic window is a simulator window, which will simulate the exact working in field and reflect the process values, alarms and message to the master control and the operator in the field. A particular situation is indicated by annunciator messages and operator message with alarms. Desalting Plant control graphic window that will monitor the entire plant is shown in Figure

8) Here ON and OFF are the control switches for plant control. The CGW shows the process in pictures and indications with tag names.

VI. RESULT AND DISCUSSION

The problems faced with PLC and how it was able to overcome by implementing DCS are explained here below;

1) Continuity of Process:

In case of motor control block, PLC does not provide any redundant system when sudden break down of motor control hence PLC will not assure continues process. DCS is well known for its redundancy technique, it provides another motor control with bypass in case of any shut down of first motor control.

2) Control Logic Execution time:

Since PLC has ladder logic programming for all the control loops, whose execution takes more time as the program flows line by line. DCS is flexible, easy in programming and execution time is less when compared to PLC.

3) Flexibility:

Once the entire setup is ready using PLC one cannot change it, if any change is required then the entire setup has to be replaced and it is very costly, whereas DCS has standard algorithms in the form of blocks which are ready to use and debug easily.

4) Data Handling Capacity:

PLC control system becomes complex in terms of software and hardware configuration as the process becomes complicated, whereas DCS can handle vast amount of process data and can be configured without major changes in software and hardware architecture.

5) Programming & Monitoring:

PLC control system will helps only in developing the programming part for control loops and for monitoring purpose it uses separate software called SCADA. But in the case of DCS control system, the programming and monitoring is done in the same software.

VII. CONCLUSION

- Following conclusions are made from the research work on adopting DCS to the desalting process; The DCS system gives a clear view of performance of the plant and its control which is enhanced due to the concept of decentralization and redundancy.
- The real time execution of control is communicated between DCS and field station is done through various field control instruments.
- The DCS system is ensured with safety such that even any one of the stations is failed, the other stations in the field will be working without interruption.
- After implementing the DCS system, overall efficiency of the plant control and quality of the crude oil has improved.
- The desalting process controlled using DCS enables to manage the process as a complete system, with control over the various sub systems.

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